

## Energy Mapping of Material Charging Process for Water Base Paint Manufacturing Industry in India

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**Abstract:** For a paint manufacturing plant with variety of water base paint products it is difficult to set standards of specific power consumption (SPC) for each process. In this paper a technique to quantify the SPC of material charging process for water base paint with the help of simple tool of Microsoft Excel is discussed.

**Keywords:** -paint manufacturing, material charging process, specific power consumption, Microsoft Excel

### I. INTRODUCTION

Paint manufacturing is one of the chemical processes that involve extreme precision of material composition (% w/w). In order to pass the quality check of finished paint product the viscosity and density are sublimetest quantities; and these quantities depend on 3 major constraints: Composition mix, grinding time and mixing time. For energy managers in large scale (Above 250KL/day) paint manufacturing plant (PMP) it is a cumbersome job to manage composition precision of each material mix and optimal power consumption for material transferring. For more than single charging line for raw materials with different physical state, time management in storage, conveying and transferring is necessary for standardizing batch production time. For the study of paint manufacturing system, a n Indian based paint manufacturing facility was appointed. It is to be noted that paint industry is one of the chemical industries where geographical and climate conditions affect the quality and consumption of powers since physical properties of major ingredients involved in paint composition are temperature and moisture dependent.

### II. WATER BASE PAINT PROCESS

A general process flow algorithm commonly observed in water based PMPs is shown in figure 1. Twin Shaft Dispenser (TSD) is a well-known electro-mechanical grinder which is employed in most PMPs. Grinding time in TSD varies according to the desired viscosity to be achieved for the emulsion inside. The speed of both arms can be controlled using a dc drives coupled with PLC where in specific density, relative gravity and gel viscosity are taken as input variables and speed of dispenser arms as output. After desired finishing in TSD the emulsion is discharged into mixer where the anchor is shafted in and out from various predefined depths. To ensure even grinding at each level of mixer the depth of anchor for mixing is maintained [1].

It is to be seen that first 9 out of 11 processes include charging of material at different times. The material addition time of each ingredient is dependent on the batch size that is predefined by production engineer.

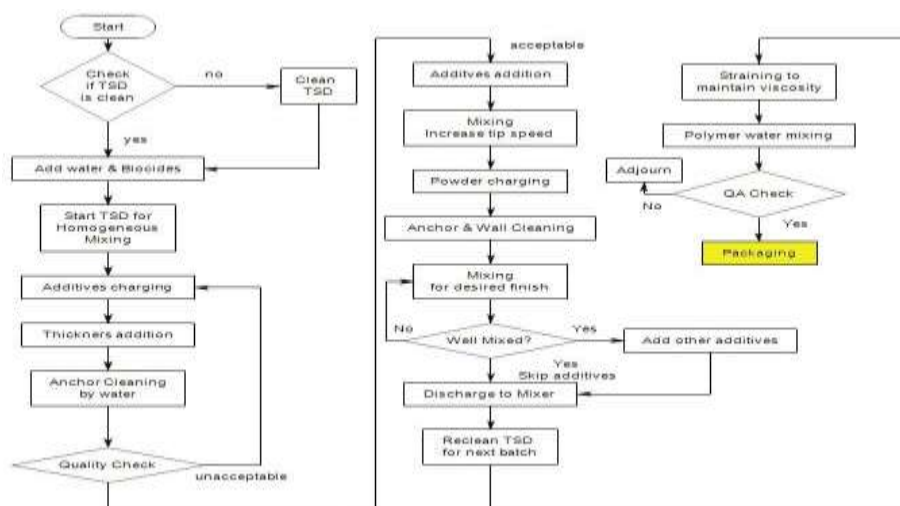


Fig.1:General Process Flow Algorithm

### III. PROCESS AND POWER MAPPING

There are 4 major processes generally classified for water base paints as follows:

- 1) Premixing operation
- 2) Raw material charging
- 3) Grinding operation
- 4) Discharging of batch

In this article we restrict to elaborate only raw material charging process. Raw material is often used layman term which otherwise can be classified into following:

- Polymorphic minerals
- Metamorphic talcs/powders
- Mineral/inorganic compounds
- Nonionic cellulose additives

Organic/inorganic colour pigments and so on. The PMP under study had three stages for charging material:

- 1) Storage from Bulk container to Silo
- 2) Silo to Weigh hopper whenever line is available and batch is planned.
- 3) Weigh hopper

to charge hopper or in or charge hopper whenever batch is to be commenced after preconditioning of available TSD.

These stages are valid when there is no immediate planning of batch, if there is an emergent need to produce any batch stage 1 is carried out directly by unloading the material truck using required capacity of transfer blower and pneumatic conveyor.

#### A. Bulk container to Silo

For former situation, stage 1 is followed as shown in figure

2. There may be group of different capacities of silos as per the requirement to store the material. Generally silo defined for specific material is not shared with other in order to avoid contamination. It is also a safe operational practice that is followed for rutile material. Major power consuming elements are Aeration blower, transfer blower and screw feeder/pneumatic conveyor. Since there is no precision of target mass required in storing the material in silo, these equipment is set to operate at rated discharge and accordingly rated power.

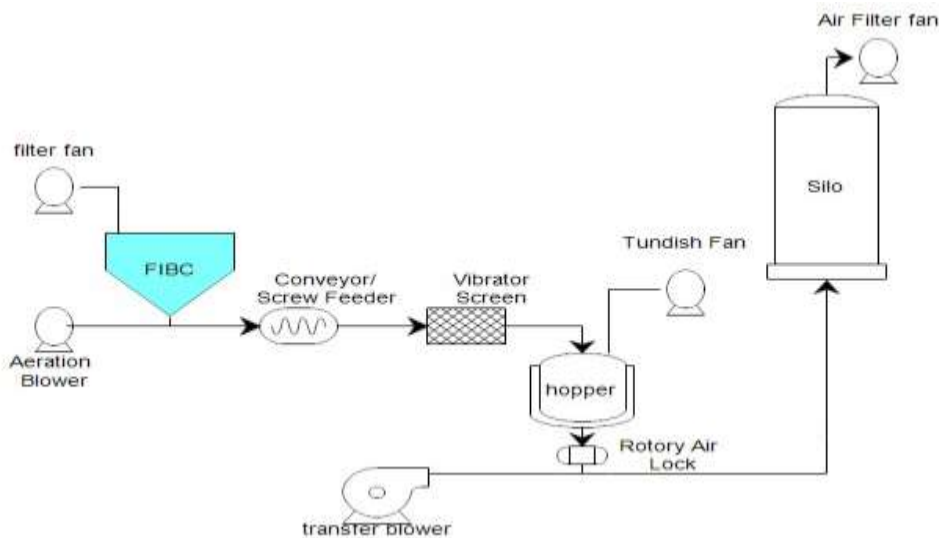


Fig.2: Storage: Bulk Container to Silo

#### B. Silo to Weigh hopper

For stage 2 as shown in 3 the materials which are ingredients in planned paint batch are extracted in required mass so as to keep the accurate composition (% w/w). These precision in extraction and conveying is maintained by Ziegler-Nichols method of Proportional Integral Derivative (PID) control of Rotoflo and speed of conveyor [2]. This technique is discussed in detail in next section. As per the availability of clean charging line and physical position of available Weigh hopper these selection of screw feeder and its power is set. Major power

consuming elements are Rotoflo and pneumatic conveyor/screw feeder which are operated on Variable Frequency Drive (VFD) to optimize power [3].

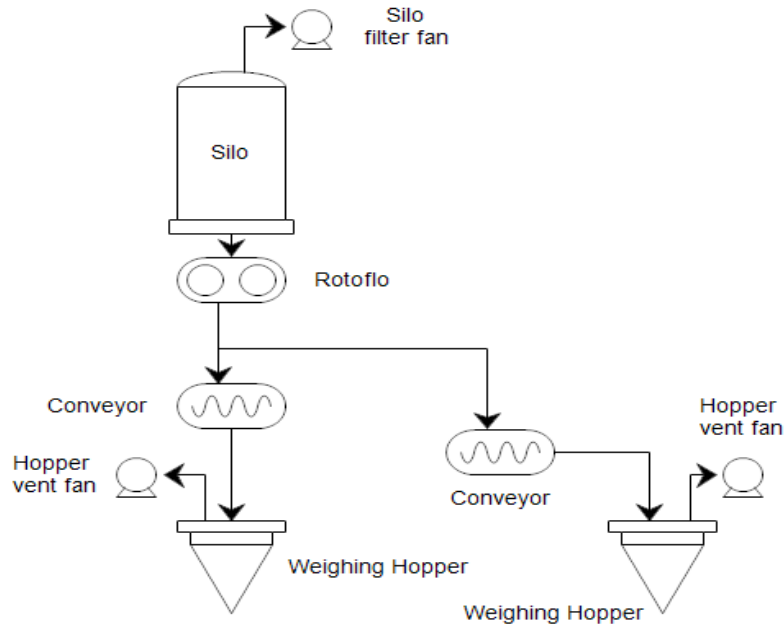


Fig.3: Stage: Silo to Weigh Hopper

C. Weigh hopper to Charge hopper

Each recipe ingredient is preweighed in the weigh hopper beneath the silo from which it is supplied prior to transfer. At completion of transfer each ingredient is checked weighed in the charge hopper. Charging of bulking ingredients to the charge hopper may commence as soon as the target TSD is selected. Bulking ingredients are then discharged to the TSD at the appropriate point within the mix and at a rate as defined within the recipe schedule. The major power consuming elements as shown in figure 4 are aeration blower and screw conveyor. A transfer blower may also be connected to provide necessary motive force if the arrangement is non-gravimetric.

The above discussed process stages are mainly for bulk handling of material. Other minor processes for handling like pigment charging and minor ingredient charging are not considered for the study as its power contribution is found less than 4%. Valves other than RAL used at different positions in the figures are not depicted for the sake of reducing the complexity of diagrams.

IV. CALCULATION OF SPECIFIC POWER CONSUMPTION

As we are dealing with material in powdery form the control of their discharge is done by controlling three main power utilizing machines, they are:

- 1) Pneumatic conveyor
- 2) Rotoflo
- 3) Rotary Air Lock valve

Major constraints that affect the discharge of material are as follows:

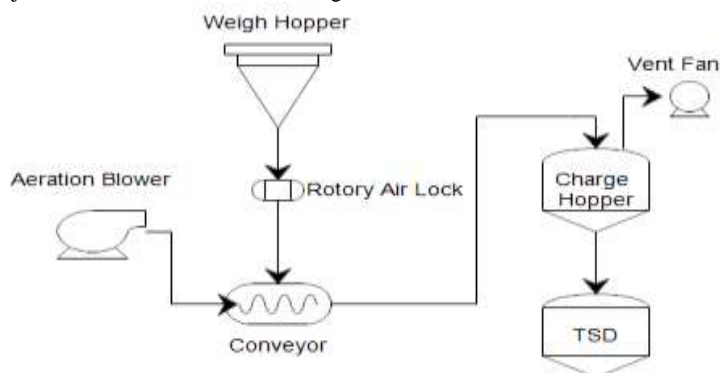


Fig.4: Stage: Weigh Hopper to Charge hopper

- Designated Material
- Conveying pressure of silo
- Rotoflo full speed setpoint
- Rotoflo trickle speed setpoint
- Hopper discharge screw full speed setpoint
- Inflight allowance
- Conveying pressure for charge hopper filling
- Trickle feed allowance

For process stage Silo to weigh hopper which is critical to bulk handling, the PID control to above list ed machine is necessary. The control must establish lean pneumatic conveying which is considered to be high energy efficient [4].

Consider the below given example for calculating SPC of material charging process:

6 raw materials are ingredients in a recipe of paint product named ABC<sup>1</sup>. Table 1 briefs the information of ingredients for charging of material X1 in M1 quantity, from FIBC to silo, energy calculation is done as follows:

**TABLE 1: Paint product material data sheet**

Raw material	Density (kg/m <sup>3</sup> )	Ingredient weight (kg)	% w/w
X1	580	M1= 1061	7.04
X2	290	M2= 566	3.76
X3	463	M3= 1415	9.38
X4	482	M4= 2830	18.78
X5	836	M5= 4670	30.99
X6	970	M6= 4529	30.05

If these calculations are considered per hour per ton of material then, the specific power consumption is said to be kW/ton. Now, if the calculations are repeated for each material charging then,

$$P_{11} = \sum_{i=1}^8 t_1 a_{1i} \text{ kWh} \quad (1)$$

Where,  $a_{11}$  = measured power of FIBC filter fan,  
 $a_{12}$  = measured power of aeration blower,  
 $a_{13}$  = measured power of screw feeder,  
 $a_{14}$  = measured power of vibrator screen,  
 $a_{15}$  = measured power of rotary airlock,  
 $a_{16}$  = measured power of tundish fan,  
 $a_{17}$  = measured power of transfer blower,  
 $a_{18}$  = measured power of silo air filter fan

And if it is time taken to convey material from FIBC to silo it is to be observed that time taken by each machine will be same as each of it is operating simultaneously. Similarly for process stage Silo to Weigh Hopper, energy calculation is done as follows:

$$P_{12} = \sum_{i=1}^8 t_2 a_{2i} \text{ kWh} \quad (2)$$

where,  $a_{21}$  = measured power of pneumatic conveyor,  
 $a_{22}$  = measured power of vent fan,  
 $a_{23}$  = measured power of Rotoflo,  
 $t_2$  = Time taken for conveying and hopper filling

And, for process stage Weigh hopper to charge hopper, energy calculation is done as follows:

$$P_{13} = \sum_{i=1}^8 t_3 a_{3i} \text{ kWh} \quad (3)$$

where,  $a_{31}$ =measured power of rotary air lock,  $a_{32}$ =measured power of pneumatic conveyor,  $a_{33}$ =measured power of aerator on blower,  $a_{34}$ =measured power of silo aeration blower,  $a_{35}$ =measured power of transfer blower,  $a_{36}$ =measured power of vent fan,  $t_2$ =Time taken for conveying and hopper filling Thus energy consumed in charging X1 is,

$$P_1 = P_{11} + P_{12} + P_{13} \quad \text{kWh} \quad (4)$$

Thus, the specific energy consumption of material X1 is,

$$E_1 = \frac{P_1}{M_1} \text{ kWh/kg} \quad (5)$$

If these calculations are considered per hour per ton of material then, the specific power consumption is said to be kW/ton. Now, if the calculations are repeated for each material charging then,

$$S = \frac{\sum_{i=1}^6 E_i}{\sum_{i=1}^6 M_i} = \frac{E_{total}}{M_{total}} \text{ kWh} \quad (6)$$

Hence,  $S$  in kW/ton is the specific power consumption for ABC paint product.

## V. BENCHMARKING

Due to several practical issues the energy consumed as per designed charging system is challenging.

Thus a benchmark is to be set which is considered to be a trade-off between design power consumption and actual power consumption. In order to establish the benchmark, an activity to test the system at various set of parameters for individual process stages and for each raw material was conducted. The first process stage i.e. from FIBC to silo, as the system is designed to operate under full load condition the operational set backs are minimalized. But, for second process stage i.e. from Silo to Weigh hopper where several quality constraints hamper the production engineer to optimize energy efficiency, the benchmarking process plays a vital role. Calculation of standard transfer time  $t_2$  and  $t_3$  is done as follows:

Let,  $t_2 = t_d$  = Design transfer time

Then,

$$t_d = t_b + t_t \quad \text{s} \quad (7)$$

Where,  $t_b$  = bulk charging time,

$$t_b = \frac{m_b}{\rho \times v_b} \text{ s} \quad (8)$$

Where,  $m_b$  = Bulk mass. The bulk mass should be within 1% error of compared to ingredient weight  $m_d$ .

$v_b$  = Discharge rate of conveyor

$\rho$  = Density of material to be charged

And,  $t_t$  = Trickle charging time

$$t_t = \frac{m_d - m_b}{\rho \times v_t} \text{ s} \quad (9)$$

Using a PID control the difference between ingredient batch mass and bulk mass is fed as a constant error signal, which accordingly sets the speed of conveyor and subsequently the discharge rate of Rotoflo valve ( $m^3/hr$ ). The conveyor speed control may be done using ac/dc drives having fast response. The conveyor pressure range must be maintained in prescribed limits. Higher conveying pressure may lead to powder fluidization with air turbulence while lower conveying pressure leads to slower charging [5]. Since with pneumatic conveying, the slip ratio is practically taken as 0.8, it should be multiplied with design transfer time.

Therefore, Standard transfer time,  $t_{ds}$ ,

$$t_{ds} = 0.8 \cdot (t_b + t_t) = 0.8 \cdot t_d \text{ s} \quad (10)$$

## VI. ON FIELD TEST TRIALS

A sample of results of field test trials is shown in table II. The material with density 678 kg/m<sup>3</sup> is transferred to weigh hopper from silo at different conveyor pressure and discharge rate of Rotoflo

valve. The main aim is to optimize the bulk charging time so that % error between ingredient target mass and actual mass is as low as possible as a result of which there is a reduction in trickle time.

**TABLE II: Test Trials for optimizing transfer time**

Density <i>kg/m<sup>3</sup></i>	Target mass (kg)	Rotoflo discharge speed (rpm)	Conveyor upper set Pressure (mbar)	%Error	Design Time (sec)	Actual Time (sec)	% increase between <i>t<sub>d</sub></i> & <i>t<sub>a</sub></i>
678	2765	950	353	0.7	350	1358	386
	2765	900	390	0.6	350	1305	373
	2765	870	390	0	350	569	163
	5439	800	395	0.02	658	1621	246
	5439	820	395	-0.1	658	1033	157

The difference between design time and actual time is because of offset in operating point between conveyor pressure and Rotoflo speed. For material with different densities the operating points for optimizing time is practically carried out by field test trials.

### VII. RESULTS

The most optimized transfer time obtained from test trails may be used as internal benchmarks for PMPs. These transfer time as further used in the calculation of benchmark SPC. The calculation is done using Microsoft Excel. Mathematical functions such as VLOOKUP and SUMIF are extensively used to filter individual material charging rate, its designated source and destination and the measured power associated with it. For the product X taken as example in the section IV the SPC results are shown in table III.

**TABLE III: Stage wise SPC**

Raw material	Stage 1 SPC (kW/ton)	Stage 2 SPC (kW/ton)	Stage 3 SPC (kW/ton)	Total SPC (kW/ton)
X1	0.47	2.34	0.97	3.78
X2	0.491	0.94	1.02	2.451
X3	0.57	1.62	1.52	3.71
X4	0.63	2.8	2.77	6.2
X5	0.624	3.81	2.65	7.08
X6	0.59	3.7	2.24	6.53

### VIII. CONCLUSION

An energy mapping technique is developed to calculate the specific power consumption of individual material that is charged to produce a paint product. From the test trials study it is concluded that optimal operating point of conveyor pressure and Rotoflo discharge is necessary for optimal transfer time. From the result stable it can be concluded that material with higher density and physical property the power consumption during material charging is affected. This technique of energy mapping is an effective tool for continuous monitoring of energy consumption and also indicative of operational issues that cause increase in SPC. The benchmark standards of SPC in this paper may be compared with international standards for same process involved and a corrective action to continuously improve benchmark and achieve energy efficient material charging system.

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